

# OTC-25861-MS

# Ship-based Carbon Dioxide Capture and Storage for Enhanced Oil Recovery

Masahiko Ozaki and Naoki Nakazawa, The University of Tokyo. Akira Omata, Chiyoda Corporation. Masao Komatsu, Mitsubishi Heavy Industries, LTD. Hiroki Manabe, Furukawa Electric Co., LTD.

Copyright 2015, Offshore Technology Conference

This paper was prepared for presentation at the Offshore Technology Conference held in Houston, Texas, USA, 4–7 May 2015.

This paper was selected for presentation by an OTC program committee following review of information contained in an abstract submitted by the author(s). Contents of the paper have not been reviewed by the Offshore Technology Conference and are subject to correction by the author(s). The material does not necessarily reflect any position of the Offshore Technology Conference, its officers, or members. Electronic reproduction, distribution, or storage of any part of this paper without the written consent of the Offshore Technology Conference is prohibited. Permission to reproduce in print is restricted to an abstract of not more than 300 words; illustrations may not be copied. The abstract must contain conspicuous acknowledgment of OTC copyright.

## Abstract

This report presents details of a proposed ship-based carbon dioxide capture and storage (CCS) method. CCS is one of the key technologies essential to achieve greenhouse gas reduction. This technology can also contribute to enhanced oil recovery (EOR) efforts by increasing oil production in mature fields. The liquefied CO<sub>2</sub> (LCO<sub>2</sub>) to be sequestered is injected directly into subseabed geological formations through a flexible riser pipe using injection facilities contained onboard an LCO<sub>2</sub> carrier ship. The primary characteristics of this LCO<sub>2</sub> subseabed injection system are as follows: the presence of LCO<sub>2</sub> injection equipment onboard the LCO<sub>2</sub> carrier ship, a direct injection into subseabed geological formations through a flexible riser pipe, and the absence of any stationary sea surface structures at the offshore CO<sub>2</sub> injection site. The advantage of ship-based transportation is flexibility in regard to *i*) multiple CO<sub>2</sub> shipping locations and storage sites, *ii*) multiple injection sites from a large CO<sub>2</sub> storage port, and *iii*) relocation of the injection site resulting from either termination of oil production or the site becoming filled with CO<sub>2</sub>. That is, ships can easily alter their shipping ports and routes to the offshore injection site(s), depending on requirements.

### Introduction

### Ship-based Carbon Dioxide Capture and Storage.

Carbon dioxide capture and storage (CCS), one of the key technologies for greenhouse gas reduction, can be accomplished by the injection of liquefied  $CO_2$  (LCO<sub>2</sub>) into geological formations, both inland and offshore in subseabeds, a method that has been studied by the petroleum industry and national organizations. The proposed ship-based LCO<sub>2</sub> subseabed injection system described herein is characterized by the presence of LCO<sub>2</sub> injection equipment located onboard the LCO<sub>2</sub> carrier ship, the

absence of any stationary sea surface structures at the offshore CO<sub>2</sub> storage site, and direct LCO<sub>2</sub> injection into subseabed geological formations through a flexible riser pipe which remains submerged on the seabed until it is pulled up and connected to the LCO<sub>2</sub> carrier ship for the LCO<sub>2</sub> injection. The main stages and components needed for the proposed system are the following: initial liquefaction of CO<sub>2</sub> and temporary storage at ports, offloading to a shuttle ship equipped with a dynamic positioning system (DPS) and injection equipment, and at the injection site, a flexible riser pipe whose ends are connected with the wellhead on the seafloor and the pickup system. The use of an unmanned offshore facility for mooring and injection results in lower facility construction/maintenance costs as well as increased safety of the entire operation. Figure 1 illustrates LCO<sub>2</sub> injection directly from the ship to the storage layer via the proposed flexible riser pipe.



Fig.1 Illustration showing direct LCO<sub>2</sub> injection from the ship to the storage layer via the proposed flexible riser pipe.

A Japanese research consortium (project director, Prof. Masahiko Ozaki of the University of Tokyo) has been studying offshore CCS since 2011 under the sponsorship of the Global CCS Institute (GCCSI). This report is a component of the *Preliminary Feasibility Study on CO<sub>2</sub> Carrier for Ship-based CCS* (2011) [1] and its follow-up study ...*Phase-2 - unmanned offshore facility* (2013) [2] sponsored by the Global CCS Institute. Other technical aspects of the study were presented in the 11th International Conference on Greenhouse Gas Control Technologies (GHGT-11) [3], [4], [5], [6], [7].

## **CCS-based Enhanced Oil Recovery.**

Currently, about 130 commercial CO<sub>2</sub>-EOR operations have been deployed around the world, with the vast majority, 123 projects by 2012, in the United States [8]. A study by Kuuskraa et al. [9] reported that i) CO<sub>2</sub>-EOR currently provides about 284,000 barrels of oil per day (bbl/d) in the U.S., equal to 6% of U.S. crude oil production, and *ii*) a total of 62 million metric tons (MMmt) of CO<sub>2</sub> was supplied to EOR operations in the U.S. in 2010. A study by Sweatman et al. [10] reported that CO<sub>2</sub> injection into oil reservoirs for EOR has been safely and effectively applied in 18,077 active wells worldwide (17,112 in the U.S.) over the past 58 years, according to the latest EOR survey (O&GJ, 2010). In addition, the report indicated that offshore CCS-EOR may be more viable than onshore options in areas where population densities are high, where offshore reservoirs are within reasonable distances from land, or where there are existing offshore oil and gas facilities and wells. A recent report prepared by the U.S. Department of Energy (DOE) [11] states that while a number of nearshore CO<sub>2</sub>-EOR pilot projects were undertaken in the early 1980s, there is not yet a commercial-scale  $CO_2$  project in the more distant offshore regions of the U.S. In contrast, a number of significant offshore CO<sub>2</sub>-EOR efforts are underway in Brazil, the UAE, Vietnam and Malaysia. This DOE report also assessed the oil recovery and CO<sub>2</sub> demand from the Gulf of Mexico Outer Continental Shelf (GOM OCS) by comparing "current" and "next generation" (improvement of oil recovery efficiency by about half) CO<sub>2</sub>-EOR technology: total 810 million barrels (MMbbl) of incremental oil and 310 million metric tons (MMmt) of CO<sub>2</sub> demand with today's moderate performance technology (Current Technology); total 14,920 MMbbl of incremental oil and 3,910 MMmt of CO<sub>2</sub> demand with the higher performing "Next Generation" technology. The CCS-based EOR projects mentioned above are summarized in Table 1.

| Authors               | CO2-EOR project                                   | Achievement/assessment                      | Remarks                      |
|-----------------------|---|---|------------------------------|
| Whittaker et al., [8] | CO <sub>2</sub> -EOR projects (worldwide)         | 130 commercial operations deployed          | Mostly in the U.S.           |
| Kuuskraa et al., [9]  | CO <sub>2</sub> -EOR production in the U.S.       | 284,000 bbl/d of crude oil                  | 6% of the U.S. crude oil     |
|                       |   | 62 MMmt of CO <sub>2</sub> supplied in 2010 | production in 2010           |
| Sweatman et al. [10]  | CO2-EOR over the past 58 years                    | 18,077 active wells worldwide               | 17,112 in the U.S.           |
| U.S. DOE, [11]        | CO <sub>2</sub> -EOR offshore the U.S.            | No commercial-scale project                 |                              |
|                       | CO <sub>2</sub> -EOR in GOM OCS future assessment | 810 MMbbl of incremental oil                | "Current" technology         |
|                       |   | 310 MMmt of CO <sub>2</sub> demand          |                              |
|                       |   | 14,920 MMbbl of incremental oil             | "Next Generation" technology |
|                       |   | 3,910 MMmt of CO <sub>2</sub> demand        |                              |

Table 1. Summary of CCS-based Enhanced Oil Recovery.

Many of the onshore injection projects in the U.S. were started in the 1970s and, thus, the pipeline transportation and injection technologies are already well established. Examples of more recent as well as planned onshore and offshore CO<sub>2</sub>-EOR projects are listed in **Table 2**. The CO<sub>2</sub> injection volumes are less than 3,000 mt/d (metric tons per day) in the U.S. onshore injection projects, except the 8,200 mt/d of the Weyburn-Midale project. Uthmaniyah (2,000 mt/d est., start in 2015) (Saudi Arabia, onshore) and Don Valley (14,000 mt/d est., under study) (England, offshore to North Sea) are both pipeline projects. The only offshore injection project currently operating is the Sleipner Project (in-situ CCS, 2,500 mt/d) in the North Sea (started in 1996). This project was the world's first demonstration of injecting CO<sub>2</sub> into a deep saline reservoir specifically for CCS, i.e., not for EOR, and remains the only development where the CO<sub>2</sub> is both captured and injected offshore [12]. The 3,000 mt/d in the present study of the proposed ship-based transportation of LCO<sub>2</sub> to offshore injection wells is greater than the injection rate of the other projects listed in Table 2, except for the Weyburn-Midale and Don Valley projects.

| Project (start year)     | Country              | CO <sub>2</sub> injection<br>(metric tons per day) | Transportation type | References                        |
|--------------------------|----------------------|--|---------------------|-----------------------------------|
| Weyburn-Midale (2000)    | USA to Canada        | 8,200  | Pipeline (onshore)  | MIT CC&ST, [13]                   |
| Coffeyville (2013)       | USA, Kansas          | 2,400  | Pipeline (onshore)  | GCCSI database, [14]              |
| Enid Fertilizer (2003)   | USA, Oklahoma        | 2,300  | Pipeline (onshore)  | MIT CC&ST, [15]                   |
| LaBarge (1986)           | USA, Wyoming         | 1,100  | Pipeline (onshore)  | MIT CC&ST, [16]                   |
| Uthmaniyah (2015)        | Saudi Arabia         | 2,000 (est.)                                       | Pipeline (onshore)  | GCCSI database, [17]              |
| Don Valley (under study) | England to North Sea | 14,000 (est.)                                      | Pipeline (offshore) | U.S. DOE, [11]                    |
| Abu Dhabi (under study)  | Abu Dhabi            | 2,200 (est.)                                       | Pipeline (offshore) | U.S. DOE, [11]                    |
| Present study            | Japan                | 3,000 (est.)                                       | Ship (offshore)     | [1], [2], [3], [4], [5], [6], [7] |

## Scenarios of Ship-based CCS/EOR

As methods of transporting  $CO_2$  from onshore to an offshore injection site, both pipelines and ships can be considered depending on the distances and costs involved. A pipeline can provide a steady supply of  $CO_2$  to the injection site, being unaffected by rough sea states. The offshore pipeline, however, cannot be relocated when oil production terminates or the injection site becomes filled with  $CO_2$ . The method proposed in this study is characterized by transporting  $CO_2$  with a relatively small-sized  $LCO_2$  carrier ship and direct injection into subseabed geological formations through a flexible riser pipe using facilities contained onboard the ship.

The advantage of ship-based transportation is flexibility in regard to the following:

- *i*) multiple CO<sub>2</sub> shipping locations and injection sites,
- ii) multiple injection sites from a large CO<sub>2</sub> storage port, and
- iii) ability to relocate the injection site in cases of the termination of oil production or the site becoming filled with CO<sub>2</sub>.

That is, ships can change shipping ports and routes to the offshore injection site as illustrated in Fig. 2.

In addition, ship-based transportation may have advantages in regard to the following:

- *iv)* cost benefit relative to a pipeline installation when the injection site is located far offshore or distant from the onshore facility,
- v) injection sites where new pipeline installation may be difficult/expensive because of the presence of obstructing bathymetric features or previously installed pipelines on the sea floor,
- vi) ability to control injection CO<sub>2</sub> volume by adjusting ship size (i.e., transporting capacity) or shipping frequency, and
- *vii)* no necessity for costly removal of pipelines in cases of the termination of oil production or the site becoming filled with CO<sub>2</sub>.



Fig. 2 Flexibility of ship accessibility to (a single/multiple) offshore injection site(s) from (a single/multiple) shipping port(s).

## Preliminary Design of the LCO<sub>2</sub>-CCS Component

#### **Design Basis of the Ship-based Concept**

The design basis is derived from the comprehensive plan developed in this study that includes transportation method, onboard cargo tank, water depth,  $LCO_2$  injection volume and design pressure of the  $LCO_2$ , as summarized in **Table 3**.

### Table 3. Design basis of the ship-based LCO<sub>2</sub>-CCS concept.

| Facility / Design parameter                 | Component/Condition  |
|---|--|
| Transport method                            | Shuttle tanker   |
| Offshore facility                           | Unmanned   |
| Injection site water depth                  | 500 m  |
| LCO <sub>2</sub> injection volume           | 3,000 metric tons per day (about one MMmt/year of LCO <sub>2</sub> ) |
| Onshore tank                                | 3,000 metric tons of LCO <sub>2</sub>                                |
| Cargo tank                                  | 1,500 metric tons per tank, 2 tanks onboard                          |
| LCO <sub>2</sub> in tanks                   | Minus 20 °C, 1.97 MPa  |
| LCO <sub>2</sub> during injection operation | 5 °C, 10 MPa   |
| Significant wave height                     | 3.0 m  |
| Current speed                               | 1.0 m/sec.   |
| Wind speed                                  | 15 m/sec.  |

## **Onshore Operations**

 $CO_2$  captured from electric power and other industrial plants is fed to the  $CO_2$  compression and liquefier facility, where the  $CO_2$  is compressed to 1.97 MPa, dehydrated, liquefied at minus 20°C, and then stored in an onshore  $LCO_2$  tank of 3,000 metric tons capacity.  $LCO_2$  is pumped from the tank through a loading arm into the onboard  $LCO_2$  cargo tanks of the carrier ship. The onshore operations from the  $CO_2$  source to delivering the  $LCO_2$  to the onboard  $LCO_2$  cargo tanks are illustrated in **Fig. 3**.



Fig. 3 Illustration: Onshore operations from the CO<sub>2</sub> source to the onboard LCO<sub>2</sub> cargo tanks.

## **Offshore Operations**

The LCO<sub>2</sub> carrier ship features, besides the LCO<sub>2</sub> cargo tanks, an onboard injection pump capable of delivering pressurized LCO<sub>2</sub> directly from the ship to the seafloor injection well through a flexible riser pipe that remains connected to the wellhead. The shuttle ship, containing about 3,000 metric tons of LCO<sub>2</sub> maintained at minus 20 °C and 1.97 MPa in two cargo tanks, is designed to be capable of injecting about 3,000 metric tons per day (about one MMmt of LCO<sub>2</sub> per year) into the target reservoir via a flexible riser pipe. At the injection site, the temperature of the LCO<sub>2</sub> pressure of 10 MPa. A combination of the heat from sea water and exhaust gas from the diesel generator is used to increase LCO<sub>2</sub> temperature in this study. First, the LCO<sub>2</sub> is heated from minus 20 °C to 5 °C by a heat exchanger using seawater with a temperature in the range from 3 °C to 8 °C; the LCO<sub>2</sub> is further heated to 5 °C using water heated by the exhaust gases of the diesel generator.

## Liquefied CO<sub>2</sub> Carrier Ship

The ship is equipped with two storage tanks of LCO<sub>2</sub>, 1,500 metric tons each. At the injection site, the ship is kept in position during the injection operation by a dynamic positioning system (DPS), consisting of one azimuth propeller (ship aft) and two side thrusters (ship fore). A simulation study was carried out under the combined disturbance conditions of wind, wave and current to determine the DPS requirements for the LCO<sub>2</sub> carrier ship. The dimensions of the ship, including DPS requirements, are summarized in **Table 4**; the ship is schematically illustrated in **Fig. 4**.

| Ship equipment         |                                | Specification     | Notes                      |
|------------------------|--------------------------------|-------------------|----------------------------|
|                        | L(overall)                     | 94.2 m            |                            |
|                        | L(pp)                          | 89.6 m            |                            |
| Hull                   | B (mould)                      | 14.6 m            |                            |
|                        | D (mould)                      | 6.9 m             |                            |
|                        | d (design)                     | 5.6 m             |                            |
|                        | Side thruster (variable pitch) | 1,150 kW          | 2 sets                     |
| Machinery              | Azimuth propeller              | 3,000 kW          | 1 set (main<br>propulsion) |
|                        | Power generator                | 3,500 kW          | 1 set (diesel driven)      |
| Ship speed (90% NSR)   |                                | 15.0 knots        | 7.7 m/sec.                 |
|                        | Capacity                       | 1,500 metric tons | 1 bi-lobe tank             |
| Storage tenk (hi lehe) | Total capacity                 | 3,000 metric tons | 2 bi-lobe tanks            |
| Storage tank (bi-lobe) | Radius of single cylinder      | 3.50 m            |                            |
|                        | Total length of each tank      | 26.96 m           |                            |

| Table 4. Dimensions and DPS re | quirements of the LCO <sub>2</sub> carrier | ship. |
|--------------------------------|--|-------|
|                                |  | Sinp. |



Fig.4 Schematic drawing of the LCO<sub>2</sub> carrier ship: two tanks, capacity of 1,500 metric tons each.

#### **Flexible Riser Pipe Pickup System and Operation**

The use of an unmanned offshore facility for mooring and injection results in lower facility construction/maintenance costs as well as increased safety of the entire operation. The flexible riser pipe, also used as a riser flow line to carry oil or gas from the seafloor wellhead, remains on the seabed and is connected to the DPS-controlled  $LCO_2$  carrier ship only after it has arrived at the ocean site. The entire pickup buoy system is shown in **Fig. 5**. This system has the following advantages over a stationary surface structure:

- no buoy system necessary for ship mooring,
- less stringent ship handling requirements than mooring at stationary surface structures, especially in rougher sea conditions, and
- the flexible riser pipe remains on the seabed in rough seas.



Fig. 5 Illustration showing the pickup buoy system components; the flexible riser pipe is connected to the LCO<sub>2</sub> carrier ship by first taking up the pickup buoy and the pickup float.

Components of the pickup buoy system are shown in **Fig. 6**. The pickup buoy is picked up first, followed by the pickup float, which is connected to the flexible riser pipe through the messenger line and the pickup wire rope. The junction of the messenger line and the pickup wire rope is kept on the seabed, using an attached sinker, except during  $CO_2$  delivery; this system isolates

the flexible riser pipe from any pickup float motions caused by waves. The pickup float, with an attached light, serves as a dan buoy (marker) for the LCO<sub>2</sub> carrier ship. The length of the pickup wire rope is 750 m, 1.5 times the water depth. The 550 m (1.1 times the water depth) messenger line is designed with sufficient mechanical strength to draw both the sinker and the pickup wire rope up to the LCO<sub>2</sub> carrier. The pickup float is designed with 10 kN buoyancy to sustain the combined weight of the messenger line and the buoy light and radar reflector.



Fig. 6 Components of the pickup systems.

## **Submerged Flexible Riser Pipe Components**

The flexible riser pipe remains submerged on the seabed until it is pulled up and connected to the LCO<sub>2</sub> carrier ship for the LCO<sub>2</sub> injection. The specifically designed components of the riser pipe as well as the design parameters are described below and illustrated in Fig. 7. The designed dimensions of the pipe are summarized in Table 5; the internal structure is schematically illustrated in Fig. 8.

- A bend stiffener is installed at the topmost part of the flexible riser pipe to limit the bend radius. \_
- The flexible riser pipe is assumed to exhibit a free catenary configuration during the injection operation.
- A pipe protector is installed around the outer sheath of the section of the flexible riser pipe that is vulnerable to wear against the seabed as a result of the motion of the DPS-controlled LCO<sub>2</sub> carrier ship.
- An anchor to counteract the tension in the flexible riser pipe to protect the wellhead equipment is installed at the touch down point (TDP), see location d. Anchor in Fig. 7.
- A bend restrictor is installed to limit bending at the joint between the riser pipe and the wellhead equipment. \_
- An umbilical cable, used in controlling the wellhead equipment and charging the batteries in the communication buoy as well as monitoring the downhole data, is bundled together with the flexible riser pipe.
- The location of the seafloor-lying flexible riser pipe is transmitted to the LCO<sub>2</sub> carrier ship by a transponder set on the pickup wire rope.



Pickup wire rope

Fig. 7 Configuration of the flexible riser pipe system and its components.

| Layer                | Thickness (mm) | Outer diameter (mm) | Material        |
|----------------------|----------------|---------------------|-----------------|
| Interlock conduit    | 5.5            | 163                 | Stainless steel |
| Inner pipe           | 6.7            | 176.4               | High density PE |
| Inner pressure armor | 2.0 x 2        | 184.4               | Carbon steel    |
| Tensile armor        | 2.0 x 2        | 192.4               | Carbon steel    |
| Buoyant layer        | 51.8           | 295                 | Plastic tape    |
| Outer sheath         | 7.0            | 309                 | High density PE |





Fig. 8 Internal structure of the flexible riser pipe.

## Economic Evaluation of CCS/CO<sub>2</sub>-EOR

## Ship-based LCO<sub>2</sub> Injection.

The economic evaluation was described in detail in a report prepared for GCCSI [2]. The cost evaluation conducted with the design basis shown in Table 3 is summarized in **Table 6** for the whole 30-year lifespan of the project. The costs were estimated using three categories; capital related cost, management cost and operational cost. The capital related cost mainly includes onshore LCO<sub>2</sub> loading facilities, LCO<sub>2</sub> carrier ship with onboard tanks, flexible riser pipe, and associated financing costs. The management cost mainly includes maintenance cost, annual insurance, satellite communication cost, and annual administration cost. The operational costs are labour wages for the operation and utility costs such as electric power, cooling water, and fuel. The total transportation costs, including onshore storage and loading as well as offshore facilities, for the transport distances of 200 km, 800 km and 1,600 km are 19.3 USD, 33.6 USD and 52.5 USD per CO<sub>2</sub> metric ton, respectively.

| Transport distance (km)                        | 200   | 800   | 1,600 |
|--|-------|-------|-------|
| Capital related cost (USD/Mt-CO <sub>2</sub> ) | 6.50  | 11.70 | 18.00 |
| Management cost (USD/Mt-CO <sub>2</sub> )      | 7.40  | 12.90 | 20.30 |
| Operational cost (USD/Mt-CO <sub>2</sub> )     | 5.40  | 9.00  | 14.20 |
| Total (USD/Mt-CO <sub>2</sub> )                | 19.30 | 33.60 | 52.50 |

#### Table 6. Summary of the total transportation cost over the 30-year lifespan.

USD/Mt-CO<sub>2</sub>: U.S. dollars per CO<sub>2</sub> metric ton.

The costs are calculated in Japanese yen in the original report. A currency exchange rate of 100 Japanese yen to one USD is used in this table.

The costs listed above include the following:

- loading section of the onshore plant: CO2 tank, CO2 loading pump, loading arm and related equipment,
- LCO<sub>2</sub> carrier ship including on-board CO<sub>2</sub> injection pump, sea water pump, CO<sub>2</sub> heater, injection control system and riser winch, and
- offshore facilities: flexible CO<sub>2</sub> injection riser and buoy systems.
- The following items are beyond the scope of the economic analysis:
  - CO<sub>2</sub> capture facilities,
  - land-based CO<sub>2</sub> gathering pipelines,
  - CO<sub>2</sub> compression and liquefier facility,
  - berth onshore,
  - CO<sub>2</sub> well head equipment,
  - pipelines between well head equipment and injection well, and
  - CO<sub>2</sub> injection wells.

### Onshore/offshore LCO<sub>2</sub> Pipeline Cost Analysis.

An example of an onshore/offshore  $LCO_2$  pipeline cost analysis is the U.S. DOE-National Energy Technology Laboratory's calculated  $CO_2$  pipeline transportation costs for the offshore Gulf of Mexico (GOM) region [11]. Their assumption of a pipeline with one Bcfd (billion cubic feet per day) of  $CO_2$  capacity traversing 100 miles (160 km) onshore and 150 miles (240 km) offshore resulted in a construction cost estimate of 1.2 billion USD for the 250 mile (400 km) combined (onshore/offshore) pipeline, i.e., 20 USD/Mt-CO<sub>2</sub>. Details concerning input parameters and calculation method can be found in reference [11].

## Applicability of Ship-based CCS for EOR in the Gulf of Mexico

The U.S. Department of Energy has recently reported on the importance of developing CO<sub>2</sub>-EOR in the GOM OCS region:

The Gulf of Mexico Outer Continental Shelf (GOM OCS) contains 1,278 discovered and proved oil and gas fields. Of these 1,278 proved oil and gas fields, 891 are active and 387 are now depleted and abandoned. These 1,278 oil and gas fields, consisting of 238 oil fields and 1,040 natural gas fields... The 238 GOM OCS oil fields contain 8,228 reservoirs with each oil field holding one to several dozen reservoirs. ... Shallow water GOM offshore oil production peaked in the late 1990s at nearly 800 thousand barrels per day (MB/D). Since then, oil production has declined to 321 MB/D in 2009 (last year of oil data from BOEM [Bureau of Ocean Energy Management] for shallow water). ...essentially all of the large GOM shallow water oilfields are mature, with only modest volumes of remaining proved reserves. As such, there is critical need for acceleration of shallow water CO<sub>2</sub>-EOR preparation and development before this large remaining domestic resource is abandoned. (Once the offshore production platform is removed, the use of CO<sub>2</sub>-EOR for storing CO<sub>2</sub> becomes much more challenging.) [11]

Although pipeline networks are well facilitated throughout the GOM, they might still be active for oil and gas transportation. For  $CO_2$ -EOR in this area, ship-based  $CO_2$ -EOR may be useful because of the following advantages over fixed pipeline  $CO_2$  transport:

- eliminates the need to build new pipelines specifically to transport CO<sub>2</sub> offshore,
- applicability of the proposed flexible riser pipe pickup system and operation for CO<sub>2</sub> injection at sites where platforms have been removed from wells (see Fig. 9 a), and
- easy and flexible access to existing oil and gas production platforms (see Fig. 9 b) from power plants and other industrial facilities along the Gulf Coast.

Figure 9 illustrates two methods of  $LCO_2$  injection: *a*) directly from the ship to the storage layer via a flexible riser pipe and *b*) through the use of a stationary structure.



a. Direct LCO<sub>2</sub> injection through a flexible riser pipe.

b. LCO<sub>2</sub> injection through a stationary structure.

Fig. 9 Illustrations showing LCO<sub>2</sub> injection from the carrier ship to the storage layer.

With ship-based LCO<sub>2</sub> transportation, CO<sub>2</sub> injection sites can be selected flexibly to optimize the displacement of oil towards a production wellbore. In addition, the ability to control the CO<sub>2</sub> injection volume by adjusting ship size (i.e., transporting capacity) and/or shipping frequency can be used effectively to create flow channels to deliver CO<sub>2</sub> to un-swept areas of a reservoir (i.e., improve control over the mobility of the injected CO<sub>2</sub>), resulting in a more productive recovery of oil production. **Figure 10** illustrates the possibility of using (a single/multiple) LCO<sub>2</sub> carrier ship(s) to access multiple injection sites to enhance oil production from a reservoir.



Fig. 10 Illustration showing oil production facilities at an oil reservoir: using carrier ships to transport and inject  $CO_2$ .

**Figure 11** shows the location of the proved fields (oil and natural gas) discovered in the GOM since 1975 [11]. Of particular interest are the oil and gas fields located in shallow water along the coast that were proved in the years 1975-1989, as they might be mature and, thus, soon to be abandoned. The proposed ship-based operation is one of the effective solutions for both CCS and EOR in this region.



Fig. 11 Location and discovery sequence for proved discovered oil and gas fields, GOM OCS [11]: To date, nearly 50,000 wells have been drilled in these fields, with 14,400 of these completions still active.

## **Summary and Conclusions**

#### i) Advantages of Ship-based LCO<sub>2</sub> Injection

The proposed ship-based LCO<sub>2</sub> subseabed injection system features LCO<sub>2</sub> injection equipment onboard a shuttle ship (3,000 metric tons LCO<sub>2</sub> load capacity) that has no need for any stationary sea surface structures at offshore CO<sub>2</sub> storage sites. The advantages of this method are flexibility in accessing onshore CO<sub>2</sub> storage and shipping sites and the ease of changing the injection site if oil production is terminated or the injection layer becomes full.

## ii) Offshore Facilities for LCO2 Injection

The proposed unmanned offshore facility for both mooring and injection features lower construction/maintenance costs and a safer operational environment than found in any manned stationary facility.

#### iii) Liquefied CO2 Carrier Ship

The ship is equipped with two  $LCO_2$  storage tanks, capacity of 1,500 metric tons each. The ship is kept in position during the injection operation by a dynamic positioning system (DPS).

#### iv) Flexible Riser Pipe Pickup System

The LCO<sub>2</sub> is injected at a rate of about 3,000 metric tons per day into subseabed reservoirs via a flexible riser pipe that connects the shuttle ship to the wellhead. The riser pickup system consists of two basic elements, besides the riser pipe: shipboard equipment such as a coupling valve, crane, winches and A-frame and offshore equipment such as a pickup buoy, pickup float, messenger line, sinker and pickup wire rope.

### v) Economic Evaluation of Ship-based LCO<sub>2</sub> Injection

The total transportation costs for offshore transporting distances of 200 km, 800 km and 1,600 km are 19.3 USD, 33.6 USD and 52.5 USD per  $CO_2$  metric ton, respectively.

## vi) Ship-based CCS for EOR in the Gulf of Mexico

Since ship-based  $CO_2$ -EOR eliminates the need to build new pipelines specifically to transport  $CO_2$  offshore, this transport method can be an effective solution for the mature GOM shallow water oilfields because of the ease and flexibility in accessing the existing oil and gas production platforms from power plants and other industrial facilities along the Gulf Coast.

#### vii) Future Work

The umbilical cable, bundled with the flexible riser pipe and supplying electricity from the ship to the seabed manifold valve, has not yet been designed. In addition, a more precise and detailed economic evaluation comparing ship-based to offshore pipeline transportation systems has to be conducted.

### Acknowledgements

The authors are grateful to the Global Carbon Capture and Storage Institute, Limited, for funding and all the institution members who worked together on the project. The authors acknowledge the suggestions provided by Mr. Eiji L. Suenaga in the preparation of this paper.

#### References

- [1] Chiyoda Corporation, Preliminary Feasibility Study on CO<sub>2</sub> Carrier for Ship-based CCS, Final Report, Global CCS Institute, October 2011.
- [2] Chiyoda Corporation, Preliminary Feasibility Study on CO<sub>2</sub> Carrier for Ship-based CCS (Phase 2 unmanned offshore facility), Final Report, Global CCS Institute, 2013.
- [3] Kokubun, N., Ko, K. and Ozaki, M. (2013): Cargo Conditions of CO<sub>2</sub> in Shuttle Transport by Ship, GHGT-11, Energy Procedia 37 (2013) 3160-3167, ELSEVIER.
- [4] Miyazaki, T., Osawa, H., Matsuura, M., Ohta, M. and Ozaki, M. (2013): Offshore Operational Availability of Onboard Direct Injection of CO<sub>2</sub> into Sub-seabed Geological Formations, GHGT-11, Energy Procedia 37 (2013) 3168-3175, ELSEVIER.
- [5] Nakazawa, N., Kikuchi, K., Ishii, K., Yamaguchi, T., Ohta, M. and Ozaki, M. (2013): Ship-based CO<sub>2</sub> Injection into Subseabed Geological Formations using a Flexible Riser Pipe Pickup System, GHGT-11, Energy Procedia 37 (2013) 3176-3183, ELSEVIER.
- [6] Ozaki, M., Ohsumi, T. and Kajiyama, R. (2013): Ship-based Offshore CCS Featuring CO<sub>2</sub> Shuttle Ships Equipped with Injection Facilities, GHGT-11, Energy Procedia 37 (2013) 3184-3190, ELSEVIER.
- [7] Suzuki, S., Nakamura, T., Muraoka, M., Higashi, S. and Ohsumi, T. (2013): Regulations on Ship Transport and On-board Direct Injection of CO<sub>2</sub> into Sub-seabed Geological Formations, GHGT-11, Energy Procedia 37 (2013) 3191-3198, ELSEVIER.
- [8] Whittaker, S. and Perkins, E.: Technical aspects of CO<sub>2</sub> EOR and associated carbon storage, Global CCS Institute, October 2013.
- [9] Kuuskraa, V. A., Godec, M. L. and Dipietro, P. (2013): CO<sub>2</sub> Utilization from "Next Generation" CO<sub>2</sub> Enhanced Oil Recovery Technology, GHGT-11, Energy Procedia 37 (2013) 6854-6866, ELSEVIER.
- [10] Sweatman, R. E., Crookshank, S. and Edman, S. (2011): Outlook and Technologies for Offshore CO<sub>2</sub> EOR/CCS Projects, OTC-21984-MS, Proc. Offshore Technology Conference (OTC), May 2-5, Houston, Texas, USA.
- U.S. DOE Report: CO<sub>2</sub>-EOR Offshore Resource Assessment, National Energy Technology Laboratory, U.S. Department of Energy, June 5, 2014, DOE/NETL-2014/1631.
- [12] GCCSI webpage http://www.globalccsinstitute.com/project/sleipner%C2%A0co2-injection
- [13] MIT CC&ST Program webpage http://sequestration.mit.edu/tools/projects/weyburn.html
- [14] GCCSI webpage http://www.globalccsinstitute.com/project/coffeyville-gasification-plant
- [15] MIT CC&ST Program webpage http://sequestration.mit.edu/tools/projects/enid\_fertilizer.html
- [16] MIT CC&ST Program webpage http://sequestration.mit.edu/tools/projects/la\_barge.html
- [17] GCCSI webpage http://www.globalccsinstitute.com/project/uthmaniyah-co2-eor-demonstration-project-0
- [18] Bureau of Ocean Energy Management (BOEM), Outer Continental Shelf: Estimated Oil and Gas Reserves, Gulf of Mexico OCS Region, December 31, 2008, U.S. Department of the Interior. Retrieved [July 2012] from http://www.boem.gov/BOEM-Newsroom/Offshore-Stats-and-Facts/Gulf-of-Mexico-Region/2011-045.aspx.